



EU TWG for Seveso Inspections & OECD
WP on Chemical Accidents
Hydrogen Fuel Risks Part 1
15 September 2023



Consequence analysis and new scenarios – dealing with specific **hydrogen fuel risks**



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Speaker Profile

- Professor of Chemical Engineering at Bologna University
- Ph.D. in Chemical Engineering
- Chair of Energy Section of the European Federation of Chemical Engineering
- Member of the Working Party on Loss Prevention in the Process Industry of the European Federation of Chemical Engineering
- Chair of the Technical Committee on Chemical and Process Industry of the European Safety and Reliability Association
- Associate Editor, Safety Science (Elsevier)
- Member of Editorial Board, Journal of Hazardous Materials and Journal of Loss Prevention in the Process Industry



Consequence Analysis & new Scenarios – Hydrogen Risk
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Outline of the presentation

1. Hydrogen and Energy Transition: new scenarios
2. Focus on consequence analysis
3. Conclusions and opportunities

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1 – Hydrogen and Energy Transition: New Scenarios

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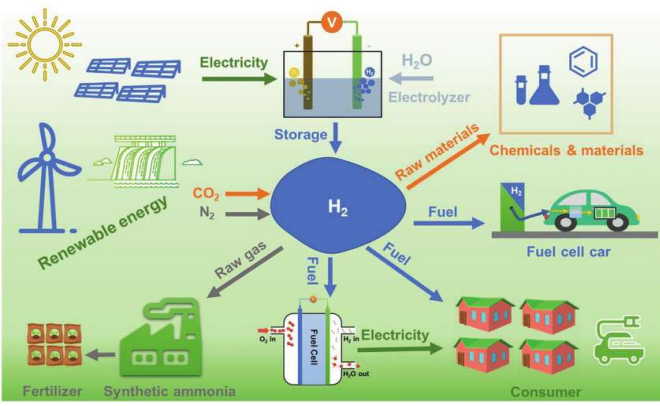
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Technologies for Energy Transition: Hydrogen

- Green hydrogen is the more important energy vector for the future energy system
- Use of hydrogen as an energy vector is proposed for both industrial and **urban / domestic** applications






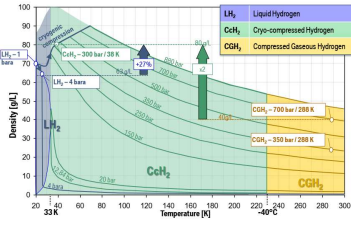
Siliper 300 - PER Module Array

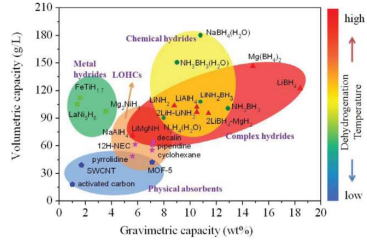
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Technologies for Energy Transition: Hydrogen Storage Systems



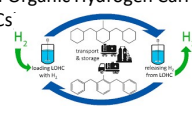


Compressed (CGH₂) – Mainstream:
Single/Multi-pressure vessel 700 bar

Cryogenic Liquid (LH₂) – Demonstration level:
Super-insulated low pressure cryotank

Cryo-Compressed (CcH₂) – Prototype level:
Super-insulated pressure cryotank (350 bar)

Liquid Organic Hydrogen Carriers (LOHCs)



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Hydrogen Safety

Molecular properties increase the risk of leak (hydrogen embrittlement)

Low minimum ignition energy (MIE) increases the risk of ignition of the flammable mixture with an oxidizer

Wide flammability range increases the risk of fire of a flammable mixture

Fuel	MIE (mJ)
Hydrogen	0.02
Natural gas	0.29
Propane	0.26
Gasoline...	0.24

Fuel	H2 concentration in air (% vol)
Gasoline vapor	~10%
Propane	~15%
Natural gas	~20%
Hydrogen	~75%

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Hydrogen Safety:
No more only a problem of “big players”

- Meeting the Paris agreement objectives requires the decarbonization of domestic applications and of private transportation
- Renewable energy technologies and energy vectors are expected to be applied outside industrial areas: in ports, airports, fuel stations, residential areas, schools...
- Operating experience with hydrogen is wide, **but limited to industrial use:**
 - ✓ Trained operators
 - ✓ Clearance areas
 - ✓ Limits to simultaneous operations
 - ✓ ATEX standards (no/limited ignition sources)

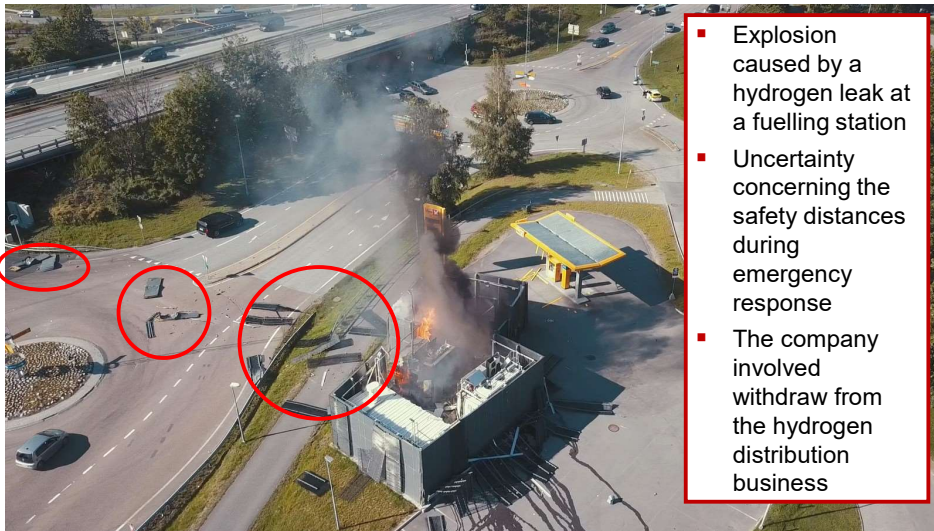
A completely different scenario is expected when the application addressed urban / residential areas

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Kjørbo, Sandvika, Norway, 2019



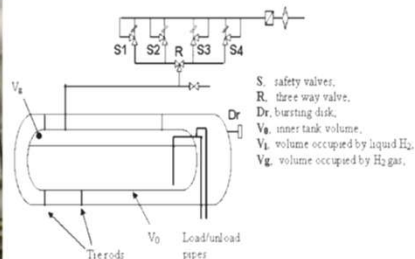
- Explosion caused by a hydrogen leak at a fuelling station
- Uncertainty concerning the safety distances during emergency response
- The company involved withdraw from the hydrogen distribution business

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Porta Susa Marshalling Yard, Turin, Italy, 1991




- Loss of vacuum in the thermal insulation layer of a cryogenic tank (42m³) for hydrogen transportation by railway
- Unignited gaseous hydrogen release from PRV
- No further consequence, tank emptied in 7 hours

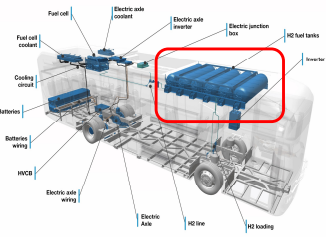
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New Hydrogen Buses in Urban Areas



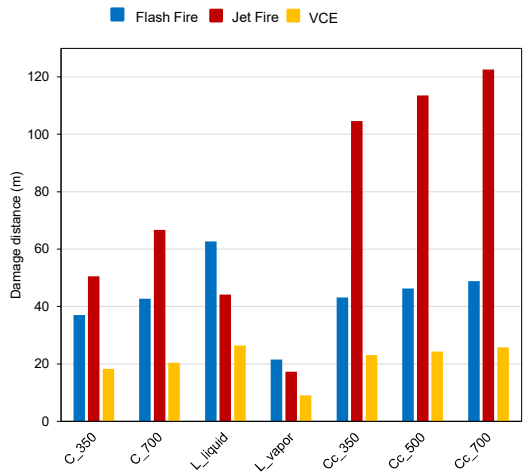
Storage technology	H ₂ physical state	Pressure (bar)	Temperature (K)	Type of tank
Compression (CH ₂)	Gas	350-700	T _{amb}	High-pressure vessels, Type III and Type IV
Liquefaction (LH ₂)	Liquid	< 10	~ 20 K	Super insulated cryogenic tanks
Cryo-compression (CcH ₂)	Gas/Liquid	350-700	66-78	High-pressure super insulated cryogenic tanks

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Damage Distances – Full bore rupture




Storage Technology	Flash Fire (m)	Jet Fire (m)	VCE (m)
C_350	35	50	18
C_700	42	65	20
L_liquid	62	45	25
L_vapor	22	18	10
Cc_350	42	105	22
Cc_500	45	115	23
Cc_700	48	120	25

- Simulation of the consequences of full bore rupture of main connection line
- Commercial or highest TRL solution considered for storage tank
- Simulations using Phast DNV 8.4, Pasquill class F, wind speed 1.5 m/s
- **Jet fire** is critical for high-pressure hydrogen; distances for CcH₂ (>100 m) are twice the ones for CH₂ with the same pressure level;



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2 – Focus on Consequence Analysis






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Consequence analysis of hydrogen releases: Pre-normative European Research



**FUEL CELLS AND HYDROGEN
JOINT UNDERTAKING**


PRENORMATIVE RESEARCH FOR SAFE USE OF LIQUID HYDROGEN
<https://preslhy.eu/home/>

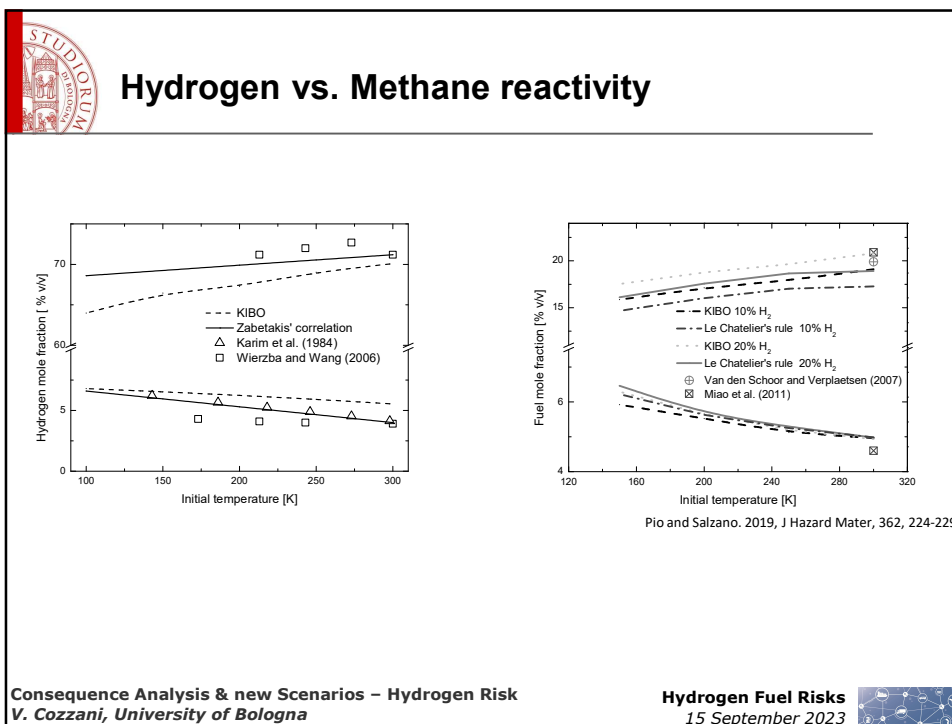
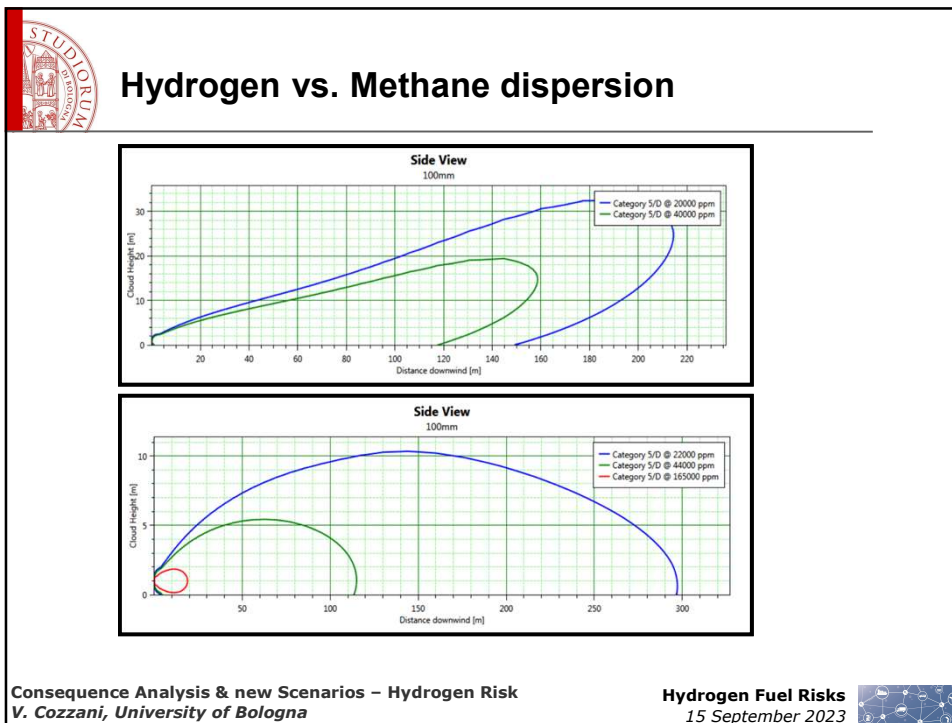
SH₂IFT project

In the following, focus limited to:

- Dispersion and reactivity
- Jet Fires
- Cryogenic vessels

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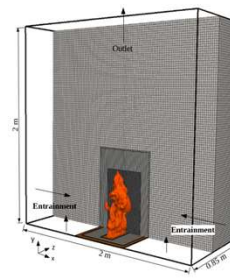
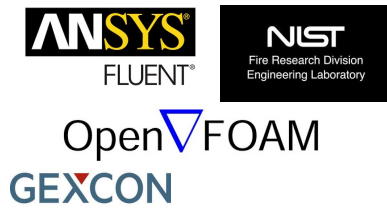






Detailed modelling: CFD

- Several CFD models can be used for the modelling of hydrogen scenarios:
- ❑ ANSYS Fluent (multi-purposes, commercial)
 - ❑ NIST FDS – Fire Dynamics Simulator (low-Mach simulator, open-source)
 - ❑ OpenFOAM (multi-purposes, open-source)
 - ❑ Gexcon FLACS – FLame ACceleration Simulator (commercial)
 - ❑ ...

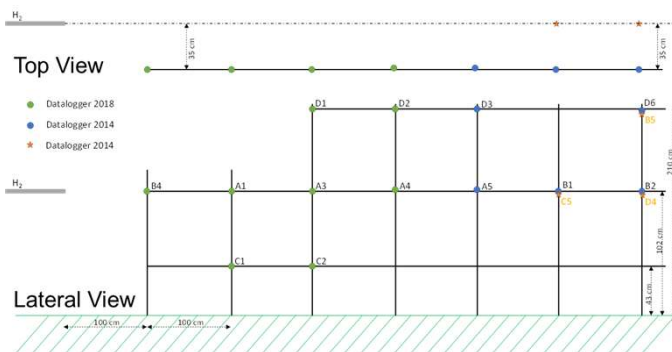


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Consequence analysis of hydrogen releases: Jet-Fire Testing




Large-scale testing, VVF Trentino experimental field, Rovereto, Italy, release of compressed hydrogen, 240 – 450 bar

Vianello et al., Chemical Engineering Transactions, 82, 247-252, 2020
<http://doi.org/10.3303/CET2082042>


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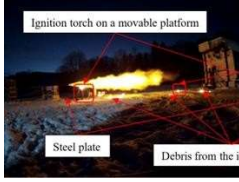
Consequence analysis of hydrogen releases: Jet-Fire Testing - SH₂IFT project



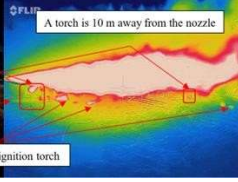
Results


Flame characteristics

Visibility decreases with daylight and when relative humidity in air is low




T = 2.5 s; RH= 95%

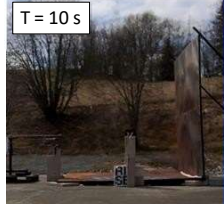




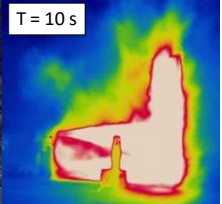
T ≈ 0 s



T = 2 s




T = 10 s



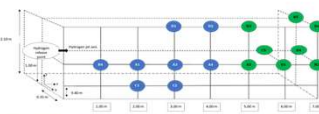
T = 10 s
RH= 60%

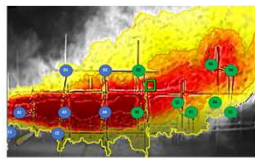
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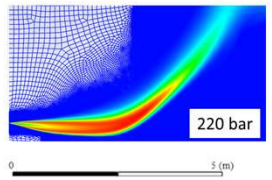
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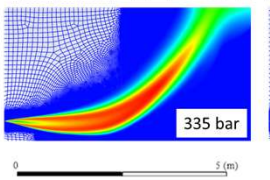
A roadmap towards risk governance in energy transition: Jet-Fire Testing



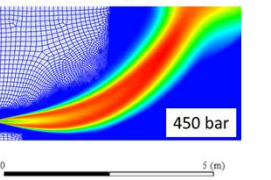




220 bar



335 bar



450 bar

CFD validation for jet-fire simulation obtained using full-scale experimental testing allows a more reliable assessment of safety distances

Vianello et al., Chemical Engineering Transactions, 82, 247-252, 2020
<http://doi.org/10.3303/CET2082042>

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STUDIORUM
UNIVERSITY OF BOLOGNA

Consequence analysis of hydrogen releases: Integral models: Miller model for jet fires

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Consequence analysis of hydrogen releases: Specific scenarios for cryogenic releases

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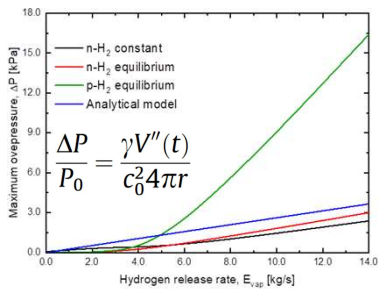
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Consequence analysis of hydrogen releases: Rapid Phase Transition Explosion



RPT test: <https://www.youtube.com/watch?v=h-EY82cVKuA>




$$\frac{\Delta P}{P_0} = \frac{\gamma V''(t)}{c_0^2 4\pi r}$$

Prevalent theory for RPT explosion is Superheat Limit Temperature

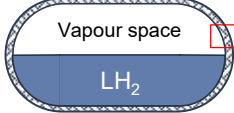
Saltano et al., 2020, Int J Hydrogen Energ, 45, 32676-32685

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Consequence analysis of hydrogen releases: BLEVE of cryogenic vessels




-253 °C

Vapour space

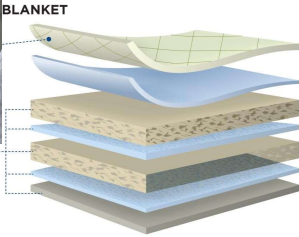
LH₂



PERLITE



MLI




BLANKET


- Tapes
- Adhesives
- Reflectives...


Cryogenic vessels are double walled and equipped with super-insulation materials

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 Consequence analysis of hydrogen releases:
BLEVE of cryogenic vessels


**Fire Exposure**




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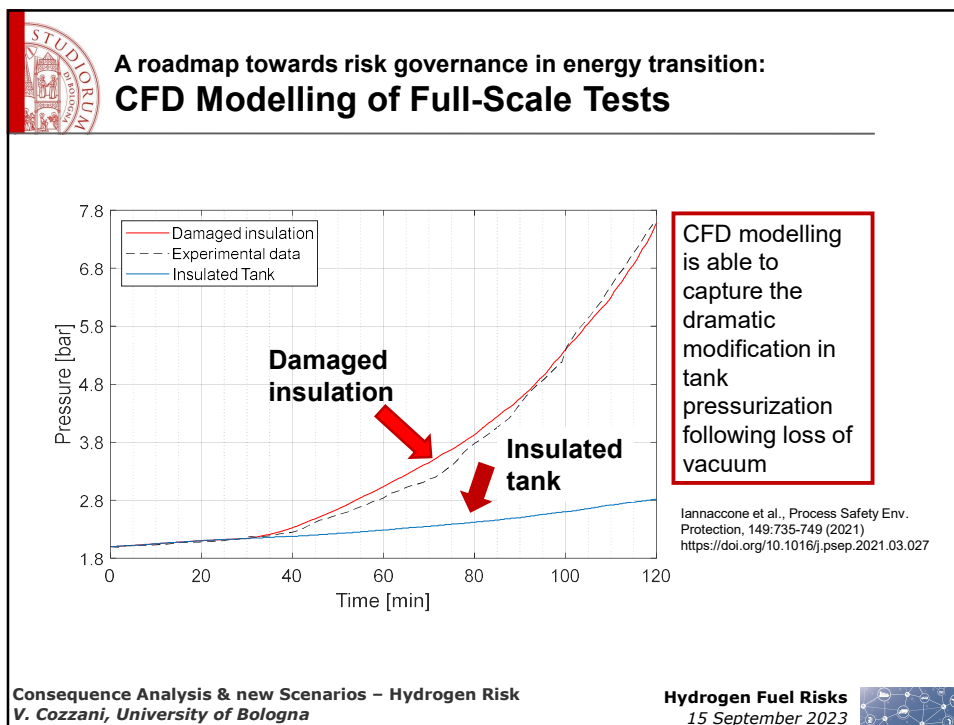
 A roadmap towards risk governance in energy transition:
Full Scale Testing

 **BAM**
Bundesanstalt für
Materialforschung
und -prüfung



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A roadmap towards risk governance in energy transition: CFD Modelling of Full-Scale Tests

CFD analysis of cryogenic tanks involved in external fires:

A. Horizontal tanks for fuel storage on ships
 B. Horizontal tanks for fuel storage on trucks


Thermal insulation: granular perlithe under vacuum

Case ID	Filling degree	Substance	Inner diameter [m]	Insulation thickness [m]	Insulation k_{tot} [mW/ (m K)]	Length [m]	Init. pressure [bar]	Init. temperature [°C]	MAWP/ MDT [bar;°C]	Nominal capacity [m³]
<i>Case A - Open-deck ship-fuel tank</i>										
A85	85%	CH ₄	4.3	0.25	300	16.5	6.0	-134.42	11.0; 50	240
A50	50%									
A15	15%									
<i>MDT: maximum design temperature, as indicated by Annex B of EN 13458-2:2002</i>										
<i>Case B - Road tanker</i>										
B85	85%	CH ₄	2.3	0.12	300	13.8	1.0	-161.49	3.0; 50	58.0
B50	50%									
B15	15%									

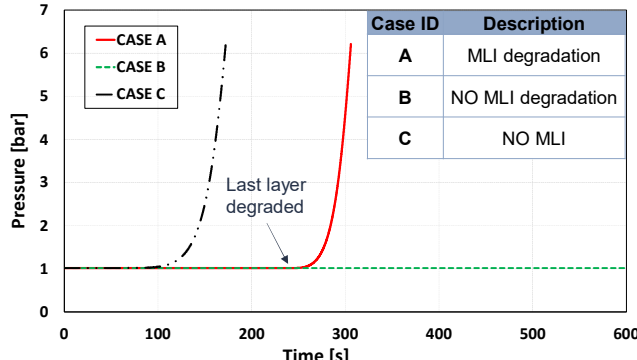
Iannaccone et al., Process Safety Env. Protection, 149:735-749 (2021)
<https://doi.org/10.1016/j.psep.2021.03.027>

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Consequence analysis of hydrogen releases: BLEVE of cryogenic vessels




Case ID	Description
A	MLI degradation
B	NO MLI degradation
C	NO MLI

- Tank response with MLI degradation (A) is similar to the one of an unprotected tank (C) rather than one with an intact insulation (B)
- 29• CASE B pressurization is negligible

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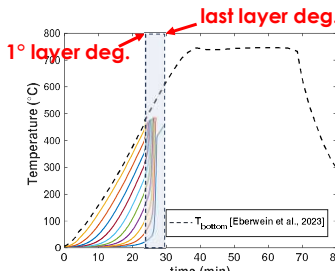
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Consequence analysis of hydrogen releases: BLEVE of cryogenic vessels


Temperature of MLI layers

last layer deg.



Before the test

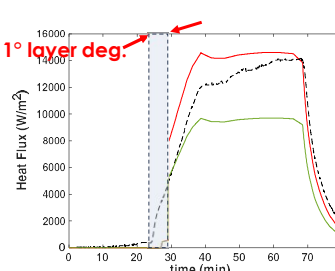
After



EBERWEIN et al., 2023

Heat flux measured vs simulated


1° layer deg.



Moment at which the heat flux measured by HTTVC strong increases is simulated pretty well by the model(a voce)


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6 – Conclusions and opportunities

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Conclusions and future perspectives


- The energy transition and the diffusion of hydrogen as an energy vector for urban and residential application is expected to strongly influence the safety of workers and population
- Specific accident scenarios are expected to become relevant due to: **new technologies, specific hydrogen properties, cryogenic applications**
- New knowledge and a rapid evolution of consequence analysis tools to support the regulatory framework is required to assure a safe use of hydrogen
- Energy transition is also an opportunity to develop and implement safer and more resilient digitalized sustainable energy technologies

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 **Acknowledgments**

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 **Thank you for attending!**

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