

MINISTÈRE DE LA TRANSITION ÉCOLOGIQUE

Liberté Égalité Fraternité

Ageing and maintenance of industrial equipment

Feedback from France



- 1. National strategy and modernisation plan
- 2. Feedback from inspection campaigns
- 3. Analysis of accidents and near-miss incidents



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Plan for modernising industrial installations (PMII 2010)



Pipes and pressure equipment

Pipeline network

Civil engineering





Safety equipment





Safety Management Systems



General methodology

- 1. To establish an **inventory** of equipment (tanks, pipes, etc.) that could lead to a **major accident** in case of failure
- To assess equipment's initial state (good, acceptable or damaged) and compile a technical dossier with all relevant information (plans, characteristics, operating conditions, photos, monitoring, repair and maintenance history, etc.)
- 3. To **develop** and **implement** an **inspection programme** to be conducted by the plant operator:
 - > Routine inspection: general state, structure, possible signs of deterioration
 - > Reinforced inspection: targeted checks and controls
- 4. To establish and maintain a data base for keeping track of and record inspection results
- 5. To carry out maintenance and repair actions

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Generic and targeted regulations

- Ministerial orders:
 - Generic requirements for monitoring ageing and carrying out maintenance
 - Generic requirements for taking ageing into account in the safety management system
 - Specific requirements for:
 - aboveground storage tanks containing flammable liquids
 - Pipelines
 - Pressure equipment and pressure vessels



Specific guidelines and targeted inspection campaigns

- Specific national working groups (trade associations, inspectors, experts, competent authorities)
- Specific national guidelines for each area of the modernisation plant:
 - How to identify relevant equipment
 - Possible failures and degradations
 - Targeted control points and associated control methods
 - Acceptance criteria
 - Monitoring frequency
 - Timeframe for repair and maintenance action / prioritisation
- Inspection checklist for plant operators



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Inspection campaigns by competent authorities

- 2012:
 - deadline for plant operators to comply with the modernisation plan.
 - First informal inspections.
- **2013 2017**: formal inspections
- Objectives:
 - To **verify** the **appropriate implementation** of the modernisation plan by plant operators
 - To **check** its **follow-up** in the long run
- Average number of annual inspections: ~300



Main compliance checks for competent authorities

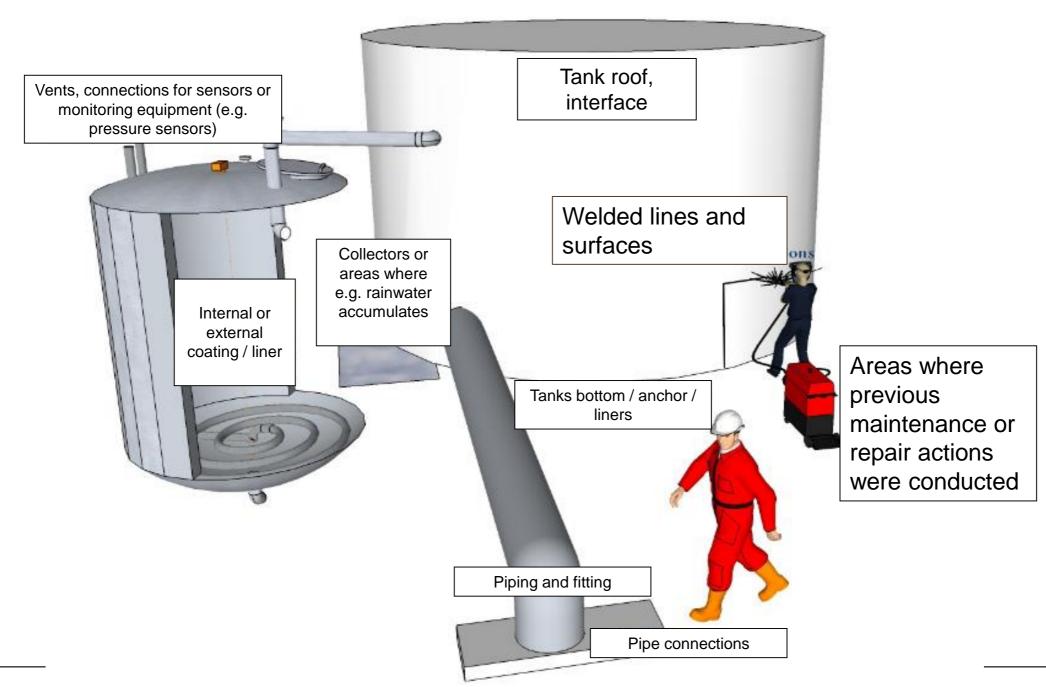
- Is the **inventory** of relevant equipment **exhaustive enough**?
- How was the assessment of equipment's initial state conducted? Is the technical dossier complete? Is it a sound basis for future assessments and controls?
- For each relevant piece of equipment, the following points are identified, checked and recorded by the operator: degradation mechanisms, acceptance criteria, control methods and frequencies, repairs
- Does the plant operator perform the necessary controls in due time? Is there a need to update monitoring and repair frequencies?







Example for storage tanks





Feedback from inspection campaign

More exhaustive and systematic identification of relevant equipment



- Improved maintenance: maintenance actions are better identified and scheduled
- Better understanding of degradation mechanisms
- Improved anticipation and organisation for maintenance and repairs

Technical dossiers are not always available, or are incomplete



- First assessment of equipment's initial state is not always (properly) done
- Maintenance or corrective actions are not always implemented (or implemented in due time)
- Outsourced maintenance: possible difficulties/issues due to outsourced maintenance are not always identified

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Lessons learnt and good practices

- Thorough and careful checks play a major role in anticipating and preventing ageing and failure of equipment
- Staff awareness and involvement: essential to involve all staff from top management to maintenance workers in the design of the modernisation programme
- Controls should be increased before and after plant shutdowns and turnarounds
- A good knowledge of main equipment types, and a good maintenance plan help anticipate the need for replacement and the management of spare parts





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BARPI and ARIA database



- Analysis of accidents extracted from the 'ARIA' database (Analysis, Research and Information on Accidents) database
- The BARPI: entity of the French Ministry for the Ecological Transition
- 57 000 summaries of technological accidents
- In France, more than 2 330 accidents or near misses involving ageing:
 - More than 1 450 in classified facilities
 - More than 645 in Seveso plants
 - About 300 in pipelines in Seveso plants (hazardous substances, gas, steam...)
 - About 100 associated with hazardous substances transportation (road, rail, sea...)



Causes of accidents involving material degradation

Corrosion: 1st cause underlying accidents involving ageing of installations







Fatigue is another recurrent cause









Accidents involving corrosion and fatigue in French Seveso plants during the last 10 years

- 215 corrosion-related accidents: 60 % relate to piping, rest to storages and tanks
- Frequent difficulties in accessing the piping to inspect their condition
- Difficulties to monitor due to the significant length of sites (or between sites)
- Causes of piping corrosion can be internal or external
- Most common cause of internal tank corrosion: defective, inappropriate or missing internal coating
- About 70 fatigue-related accidents (most commonly due to excessive vibrations)



Recurrent failures leading to corrosion

Inappropriate technical choices:

- Absence of protective coating against corrosion
- Incompatibility between products and materials
- Unsuitable ergonomics
- Dangerous installations design

Insufficient maintenance:

- Lack in maintenance
- Inappropriate non-destructive controls

Human errors:

- Default in assembly of a heat insulator
- Shock leading to the damaging of a protective coating



Possible corrective measures to manage corrosion

Improvement of operation monitoring

- Updated pipeline network map, inventory of sensitive points
- Trapdoors for inspection of thermal insulated pipes

Improvement of control procedures

- Regular thickness measurement on critical points
- Leakage tests or hydraulic tests
- Intensification of inspection programs

Modification of installations

- Use of more resistant alloys (hastelloy, stainless steel)
- Modification of protective coating material
- Removal of risky tapping
- Enslavement of equipment to safety measures

Modification of the process

- Change in parameters such as temperature, pH, product flow
- Reduction of operating pressure of equipment



Possible corrective measures to manage fatigue

Improvement of control procedures

- Increased inspection frequency
- Identification of equipments subject to the same risks than those involved in an accident
- Modification of inspection plans to take into account specific vulnerability to fatigue of some equipment
- Increased critical equipment's replacement frequency

Modification of installations and processes

- Changes in equipment design to make it more suitable for exposure to vibrations
- Changes in operating procedures to limit stresses
- Modification of operation parameters

Training

- Training of maintenance staff to the caution to be taken when manipulating sensitive equipements to limit their weakening
- Enslavement of equipment to safety measures



Fire in the distilling unit of a refinery ARIA 54828 (in 2019)

despite the French regulation « modernisation plan for industrial facilities »



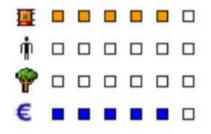


Fire in the distilling unit of a refinery

Gasoline leak and fire in the distillation unit at around 4 am on Saturday

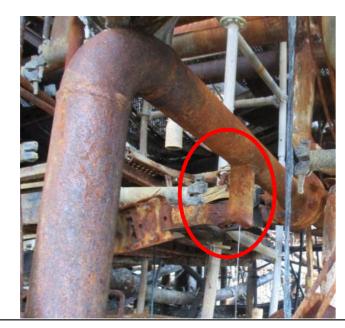
The main focus of the fire was extinguished around 8 am, the secondary focuses were extinguished until Sunday 15 December around 2 pm

Dangerous materials released
Human and social consequences
Environmental consequences
Economic consequences



400t of flammable liquids (upper threshold 50t)

based solely on estimated operating losses of approximately €171 million





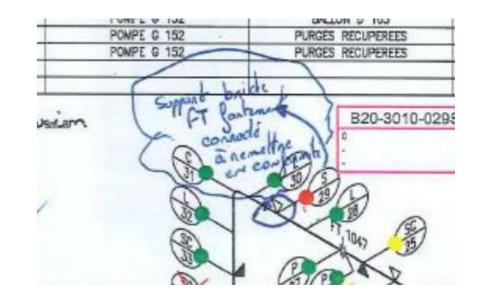


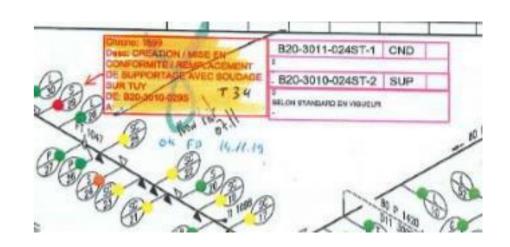


Corrosion of a pipe at a support

Support found to be visually **corroded but no inspection** of the pipe at the support due to:

- Incorrect identification of the type of support in the document base and on the isometric, leading to an inappropriate thickness measurement
- The various people working in the field do not realise that the measurement carried out (by ultrasound) is not the one that should have been carried out according to the procedure in force (gammagraphy)
- Failure to replace the corroded support
- Confusion between two substrates in the definition of the work required of the intervening company: the work is carried out on the wrong substrate
- No formal validation stage for the preparation of the work
- Acceptance of the work does not allow these errors to be corrected

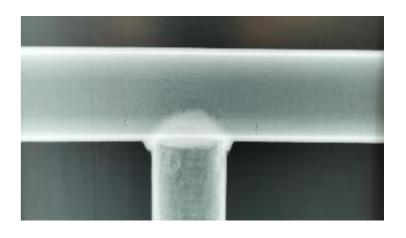






Action plan

- Survey of pipe supports in unit D11 and update of isometrics
- 61 493 items inspected
- 506 pipe supports identified in the unit
 (3 supports were not identified, 6 were incorrectly identified)
- Checking and quantifying the damage to the piping at the identified supports
 - 1 pipe shows a significant loss of thickness
 - 38 others show losses in thickness that need to be analysed
 - Replacement of pipes and supports
 - Modification of the work management and acceptance tool







Mercury rainwater tank rupture at a chemical plant ARIA 51102 (in 2018)

NO subject to the French regulation « modernisation plan for industrial facilities »





Mercury rainwater tank rupture

- Tank used for the recovery of mercury-contaminated rainwater (628 m³ capacity, steel, lined)
- Stoppage of mercury water treatment due to a reagent delivery failure
- AND heavy rainfall
- Use of a tank known degraded (since a precedent inspection)
- Internal instruction limits the filling to 60 % of its capacity
- Use of the tank to store beyond the maximum filling instruction



Lack of anticipation of degraded situations, resulting in an inappropriate overfilling decision.



134 m³ flowed into the River (a flow of 65 g with a concentration of 0.49 mg/l of mercury).



Conclusion on lessons learnt from accidents

- Problem of anticipation or detection in a timely manner (sometimes in spite of many 'warnings')
- Defective equipment or interpretation error during verification campaigns
- Insufficient temporary repairs or facility renovation programs scheduled too late
- Large-scale industrial platforms -> large number of devices or piping involved.
- Full extent of degradation possibilities + identification of factors capable of speeding the deterioration process.
- Pay attention to critical points
- Control and maintenance efforts within inaccessible zones



Thank you for your attention!

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